

The separation of metals (Cu, Cd, Zn) from acid mine drainage using hydrochar, and the regeneration of used hydrochar applying various solvents

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Goals And Objectives



Pyrolysis



Biochar

HTC



Hydrochar

To investigate the **capacity of hydrochar** as a low-cost sorbent for removing Cu, Zn, Cd in synthetic mine water

Assess the hydrochar **regeneration**

Research Methodology

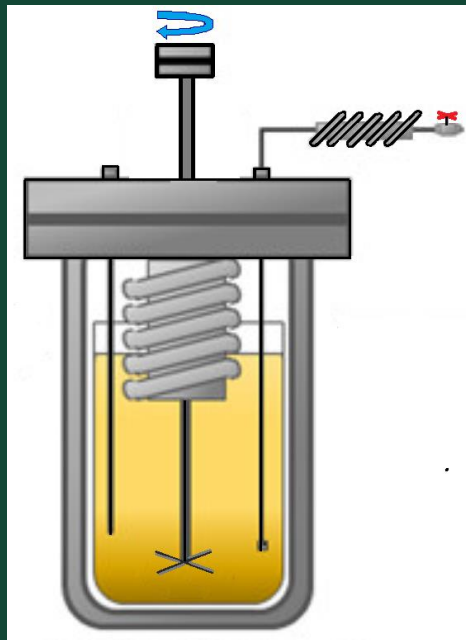
**Septage & food
waste**



Digestate



**Hydrothermal
Carbonization**



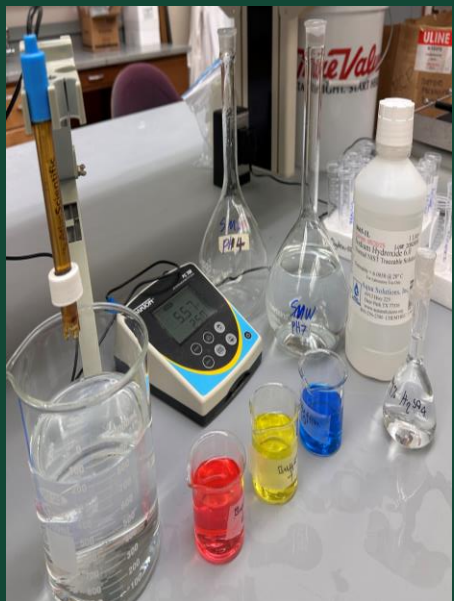
Hydrochar



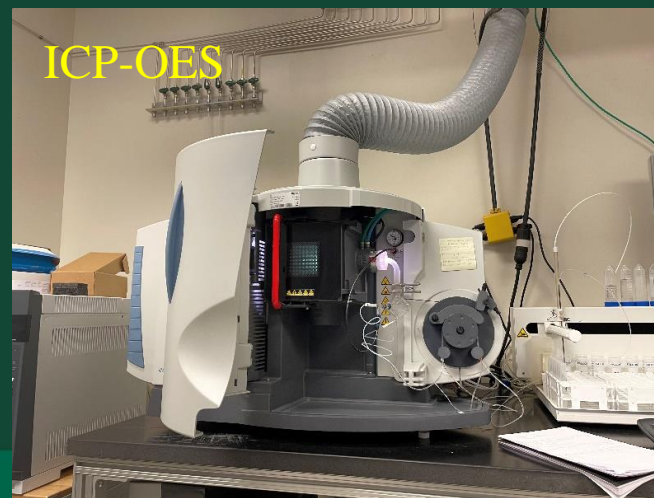
**Crushed
hydrochar < 1mm**



Research Methodology



$$\text{Removal percentage} = 100 \times \frac{C_0 - C_f}{C_0}$$



Research Methodology

- Regeneration of the heavy metals from the used dried char material leached in ethylene diamine tetra acetic acid (EDTA), HNO₃, KCl, and DI.
- Dried char mixed with solvent, centrifuged & filtered; eluent analyzed and char saved for analysis and further use.
- For each adsorption-desorption cycle, the ratio of the solution to hydrochar was kept at 7.

$$\text{Desorption percentage \%} = 100 \times \frac{C_s \times V_s}{(C_0 - C_f) \times V}$$

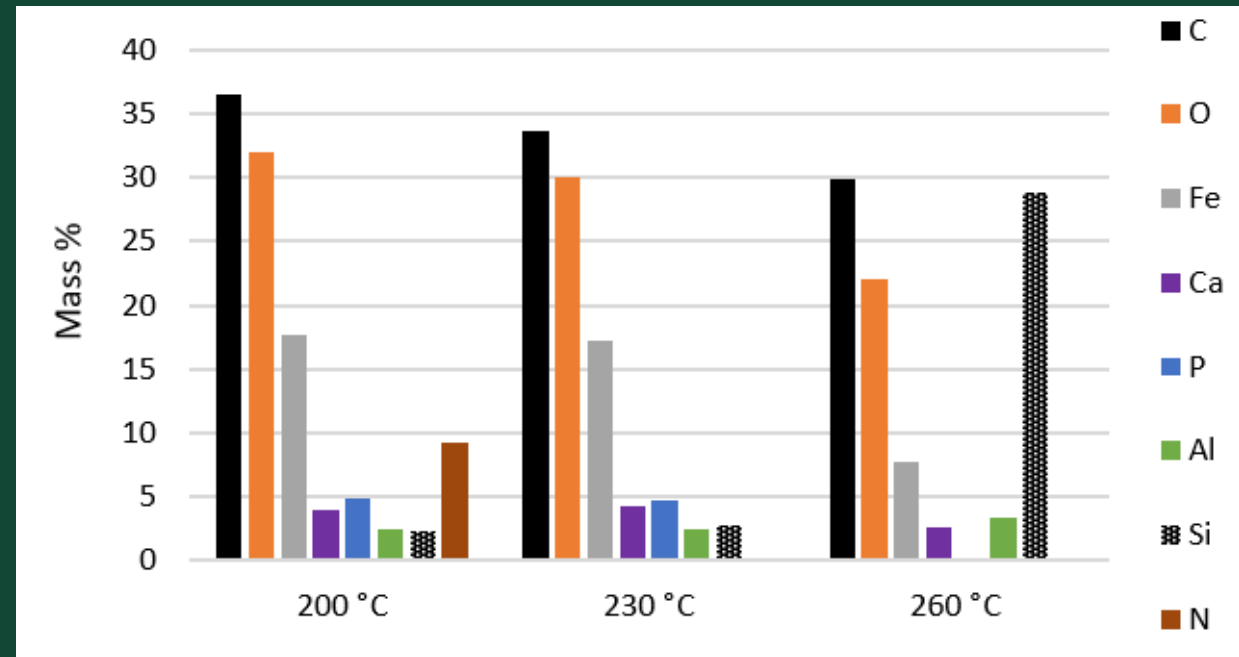


EDTA, HNO₃, KCl, and DI

Results and Discussion:

The effect of hydrochar processing temperature

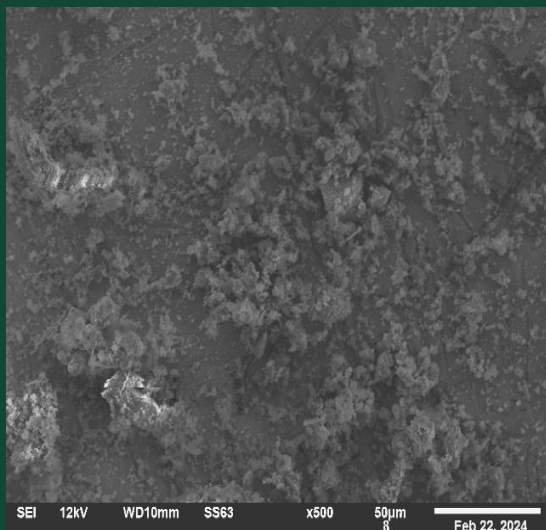
- Liu et. al reported at a higher temperature range (200–250 °C), there is an initial reduction in the oxygen and carbon content of the hydrochar (F. Liu, 2017)
- As the temperature rises from 200 °C to 260 °C, there is a reduction in the atomic ratios of oxygen to carbon and hydrogen to carbon (M. Sevilla, 2009)
- This phenomenon can be the result of the thermal-induced decomposition and volatilization of organic compounds



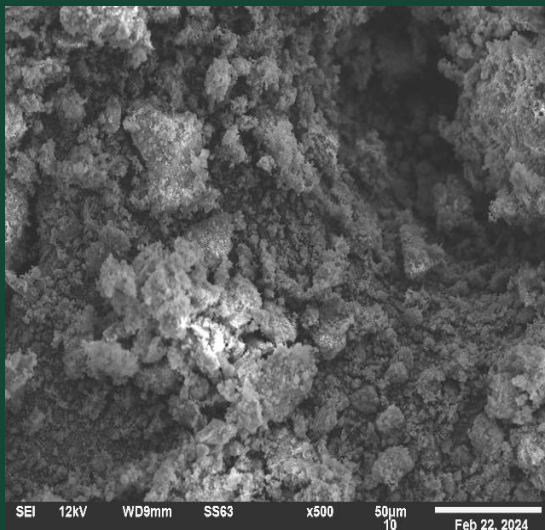
Results and Discussion:

The effect of hydrochar processing temperature

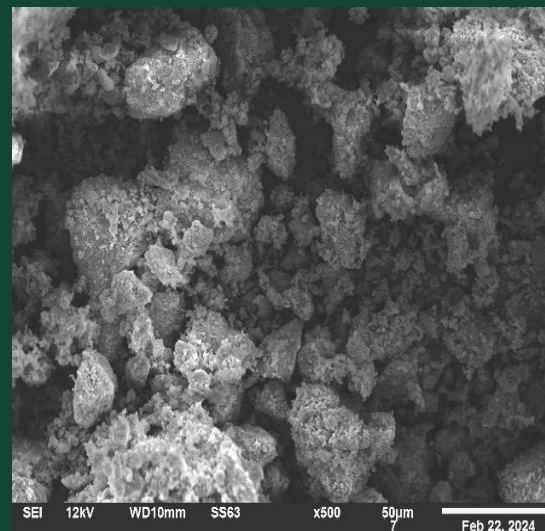
hydrochar processed at 260 °C



hydrochar processed at 230°C

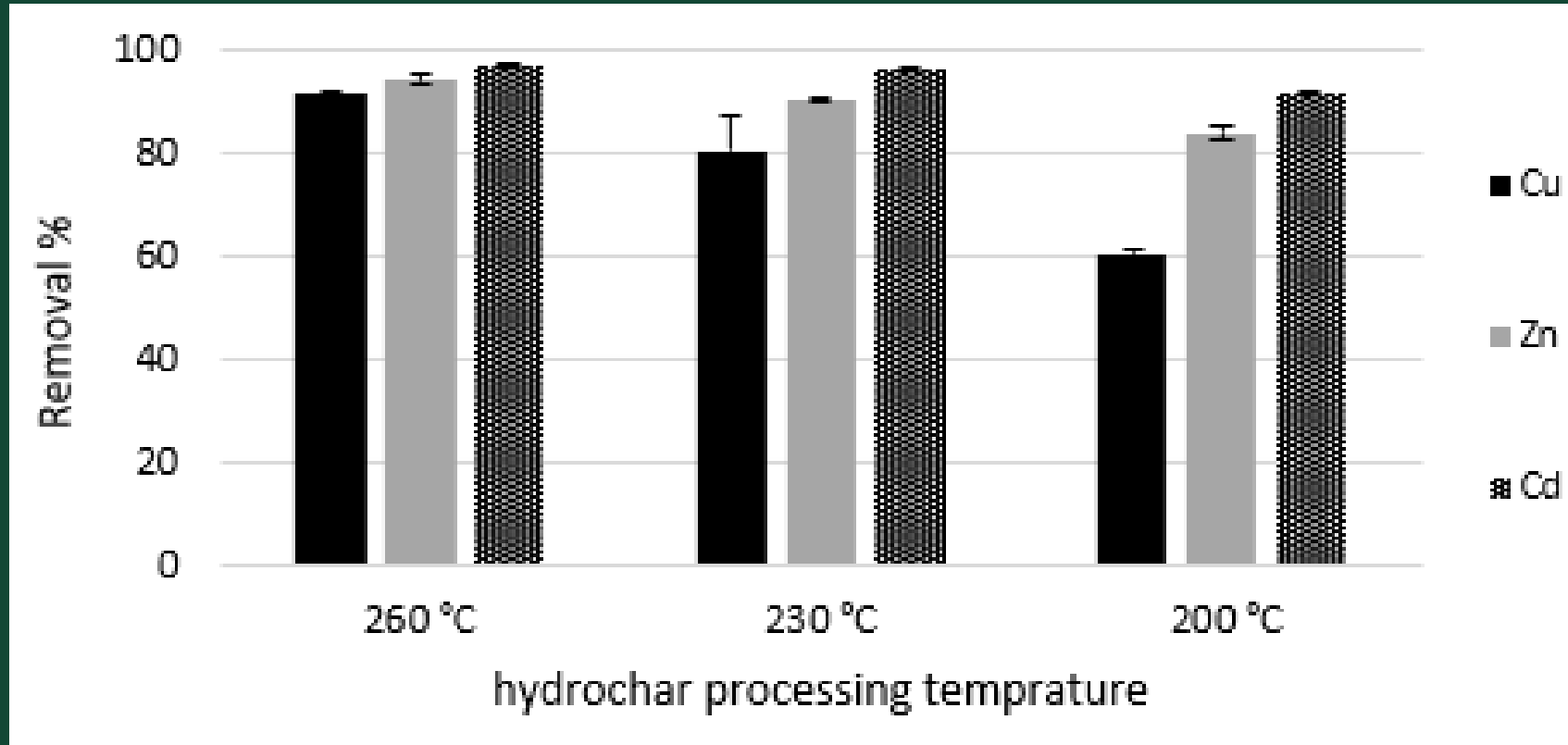


hydrochar processed at 200 °C

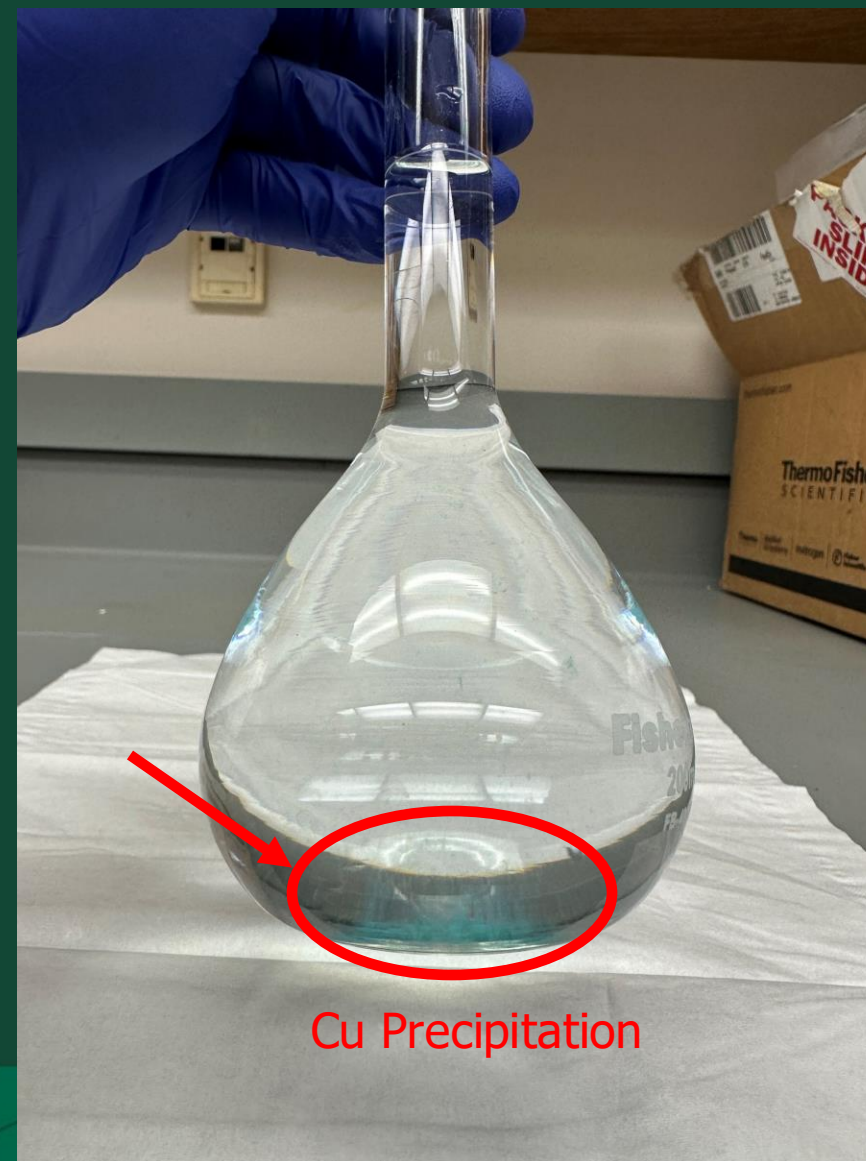
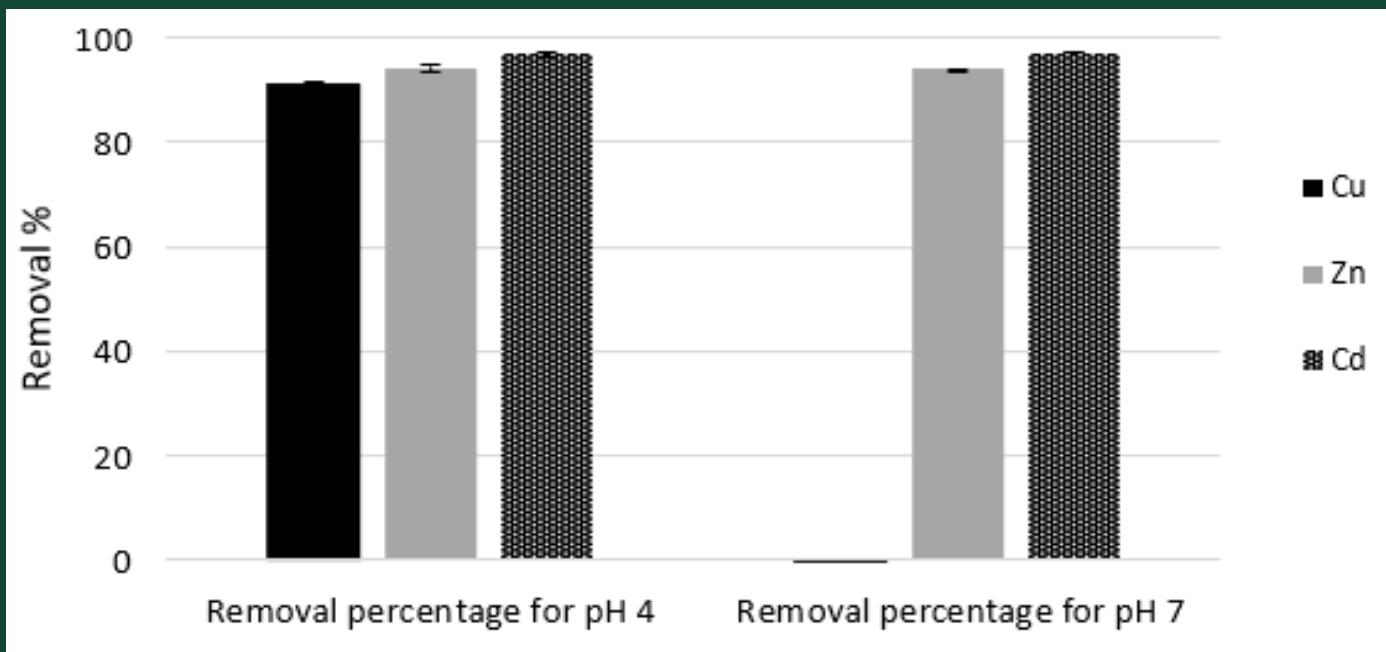


Results and Discussion:

The effect of hydrochar processing temperature

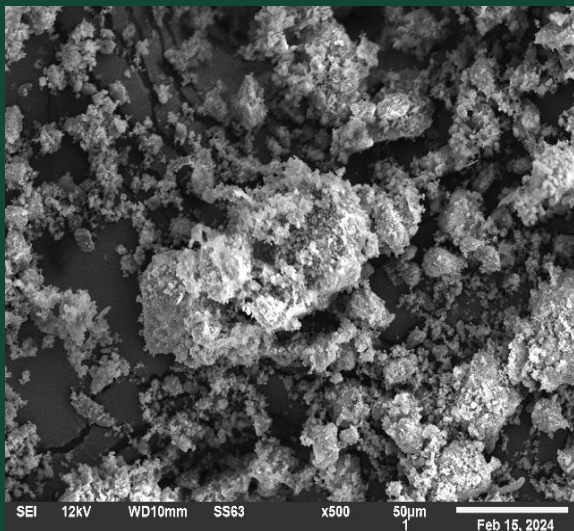


Results and Discussion: The effect of the pH of SMW

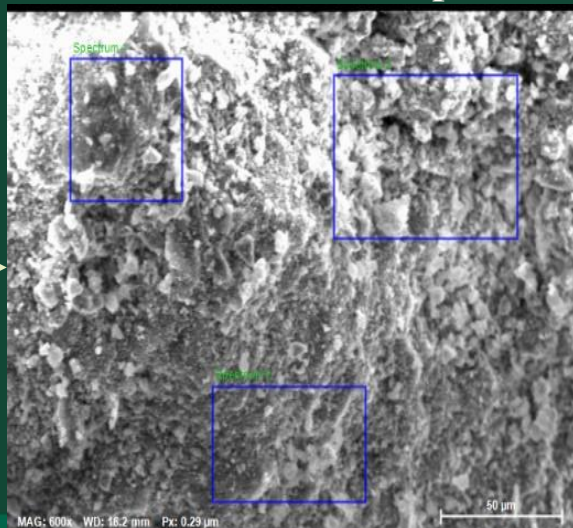


Results and Discussion: The effect of first-cycle

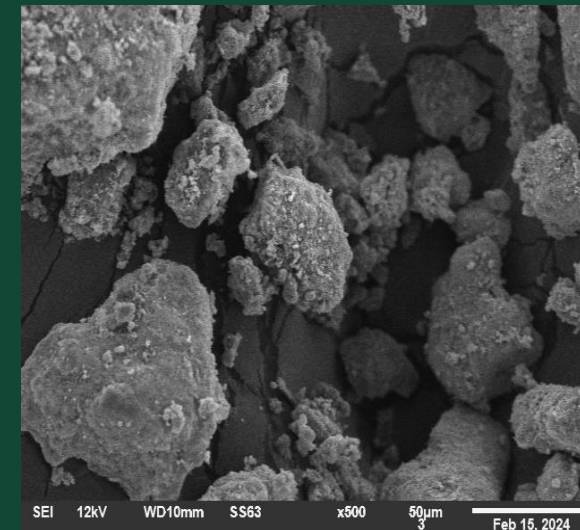
Raw hydrochar



After the first adsorption



After the first desorption by EDTA

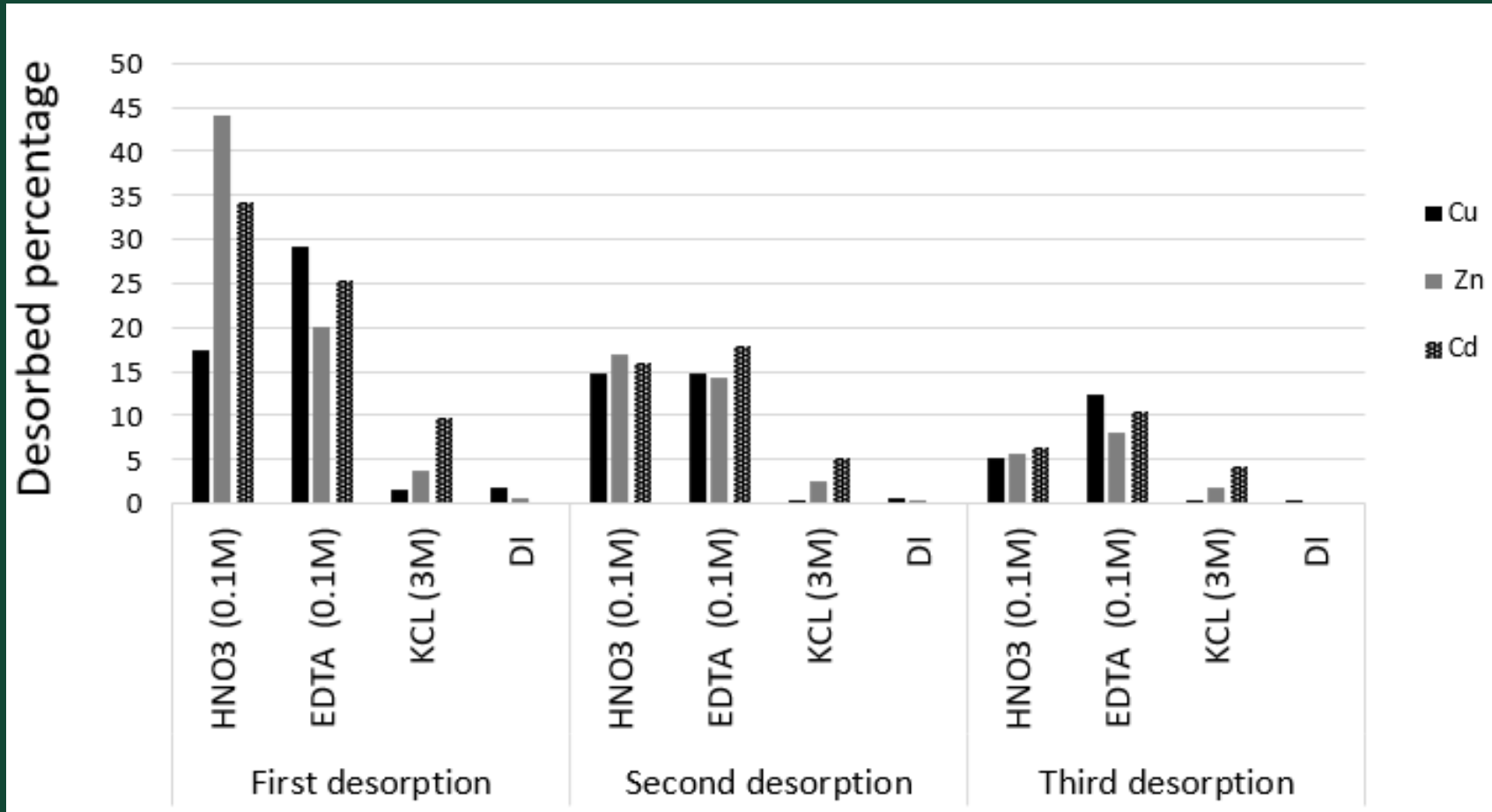


Element	At. No.	Mass [%]	Mass Norm. [%]	Atom [%]	abs. error [%] (3 sigma)
C	6	4.98	9.00	25.00	0.63
Fe	26	18.53	33.47	20.00	2.31
P	15	6.49	11.73	12.64	0.70
Al	13	3.83	6.91	8.55	0.53
O	8	2.25	4.07	8.48	0.24
Si	14	3.40	6.15	7.31	0.41
Ca	20	4.70	8.49	7.07	0.47
S	16	1.65	2.99	3.11	0.17
Pd	46	5.33	9.62	3.02	0.51
Mg	12	0.98	1.77	2.44	0.16
Cd	48	2.23	4.03	1.20	0.21
Zn	30	0.64	1.16	0.59	0.11
Na	11	0.17	0.30	0.43	0.03
Cu	29	0.18	0.32	0.17	0.03
		55.38	100.00	100.00	

Results and Discussion:

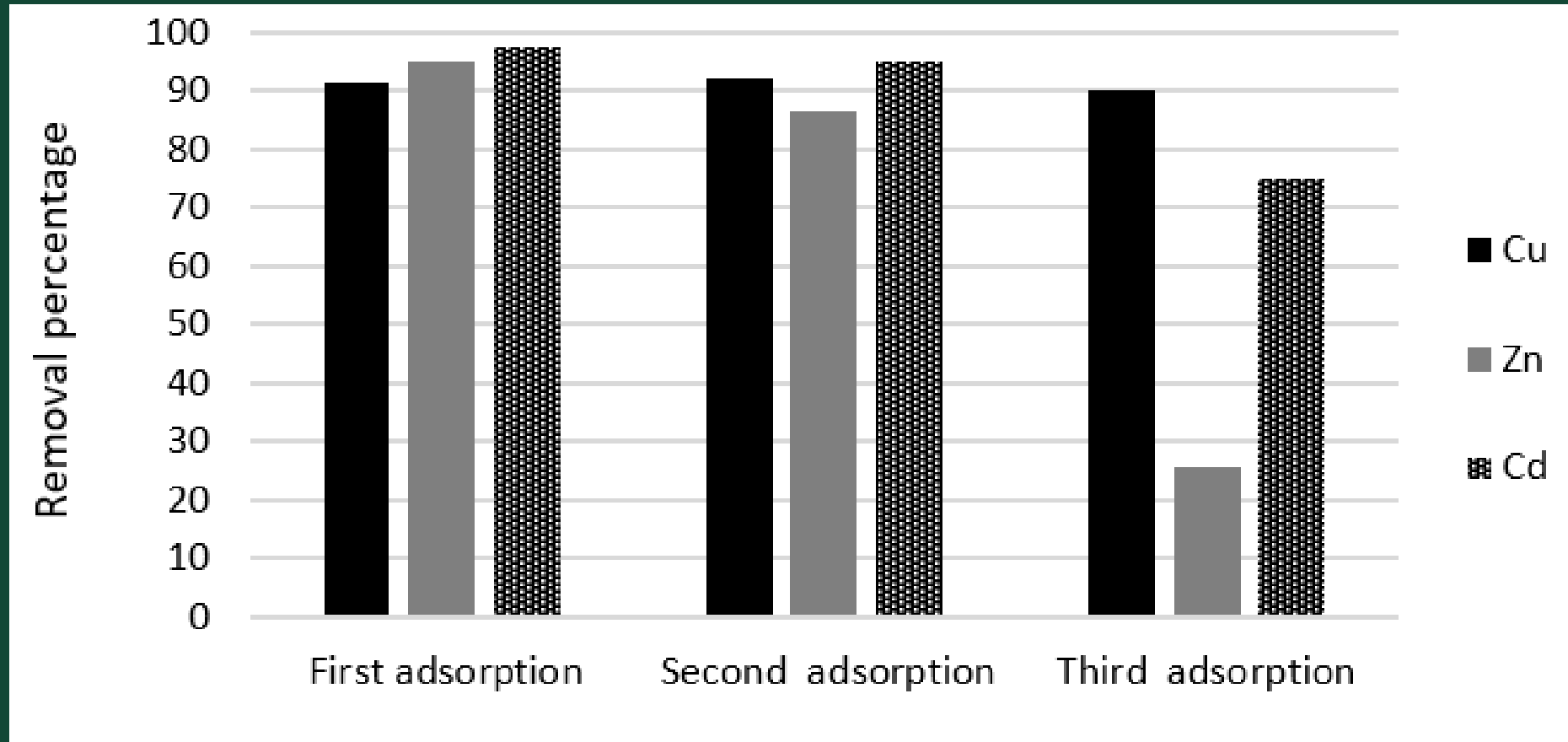
Reduction in desorption through the second and third desorption cycles

- The reduction in desorption percentage observed in subsequent cycles can be attributed to several factors such as **surface saturation, sorbent degradation, metal redistribution, ion exchange dynamics, and kinetic effects.**



Results and Discussion:

Comparison of metal removal percentage observed in subsequent cycles



Conclusions:

- The highest metal removal was obtained at pH 4 for the hydrochar processed at 260 °C.
- 5g hydrochar resulted in consistent removal percentage for Cu and Cd ions.
- As processing temperature increased, there was a notable decrease in O/C and H/C ratios. A smoother surface, and higher solubility were also observed.
- Zn precipitation observed at pH 7.
- EDTA and HNO₃ were the most effective solvents for desorption.
- KCl solvent was a less effective solvent.
- Metal removal dropped after the second desorption cycle and the material became “sludgy”.

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