

# Passive and Active Treatment of Arsenic and Antimony at a Remote Abandoned Mine Site in Idaho

Presented by

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Golder Associates, Inc.



June 4-9, 2016 Spokane, WA

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# Presentation Outline



Site Characterization

Project Overview

Identified Treatment Technologies

Bench Testing

Results

Conclusions

Path Forward

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# Site Characterization



Abandoned silver and antimony mine

No power

Limited access

Adit drainage

Remediation through the Idaho Department of Lands (IDL)





# Adit Water Quality

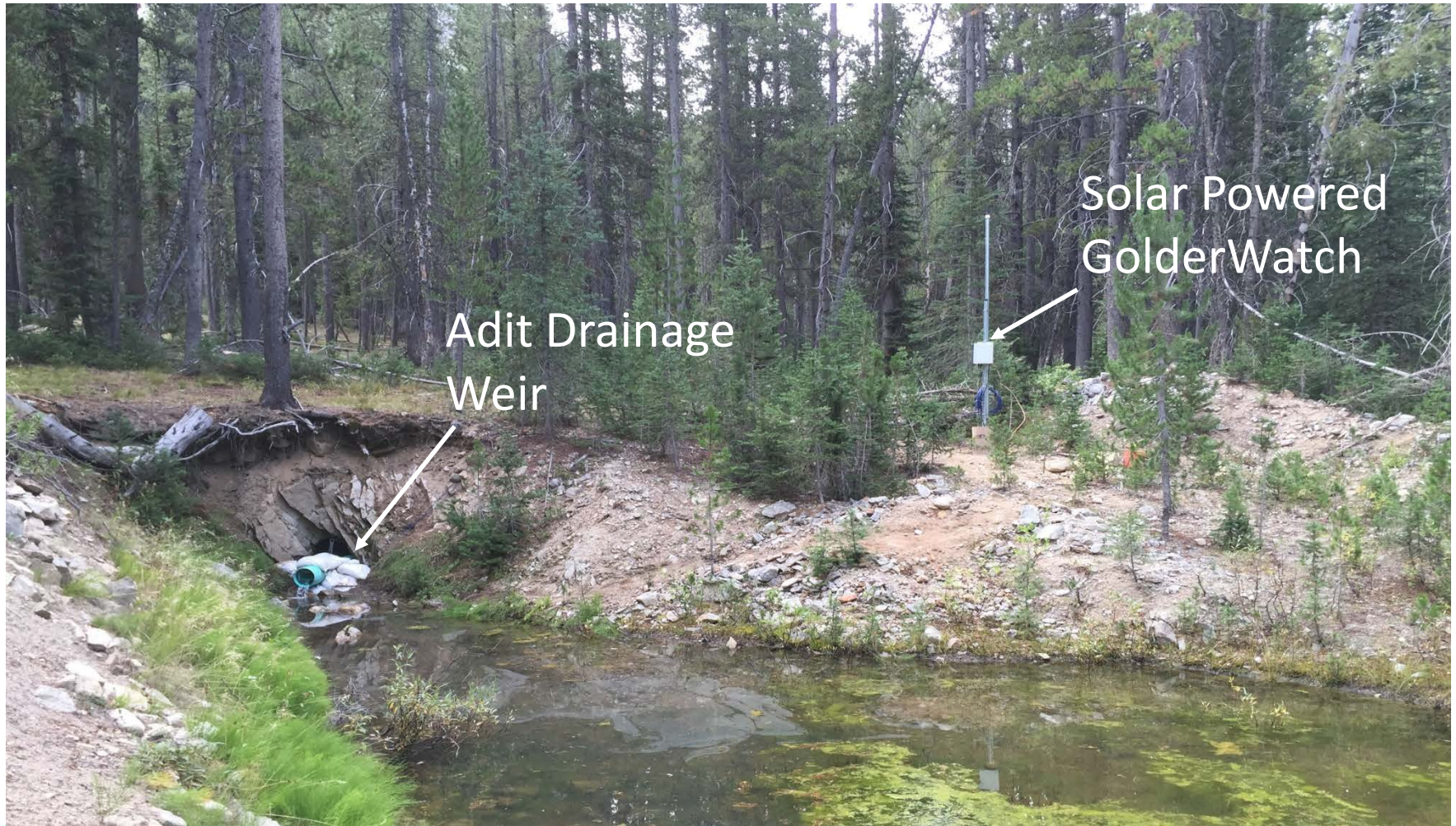
- *Low metals*
  - Iron: 0.06 mg/L
  - Aluminum: 0.14 mg/L
- *Circumneutral pH, low alkalinity*
- *Low Flow: 4- 8 m<sup>3</sup>/hr (15-30 gpm)*
- *Constituents of concern include:*
  - Arsenic and Antimony



Parameter	Influent Concentration	Effluent Targets			
		EPA MCL	Required Removal, %	IDAPA	Required Removal, %
Antimony, total, mg/L	0.069	0.006	91%	NS	NA
Arsenic, total, mg/L	0.163	0.010	94%	0.150	8%



# Site Monitoring Setup



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# Project Overview



## Project Goals

- Meet IDAPA or EPA MCL standards
- Screen technologies based on efficiency in removing arsenic and antimony
- Narrow down implementation of effective technologies in a passive or semi-passive configuration



# Treatment Technologies



## Passive

- Aerobic Wetland

## Active

- Iron Co-precipitation
- Media Absorption





# Bench Testing: Aerobic Wetlands



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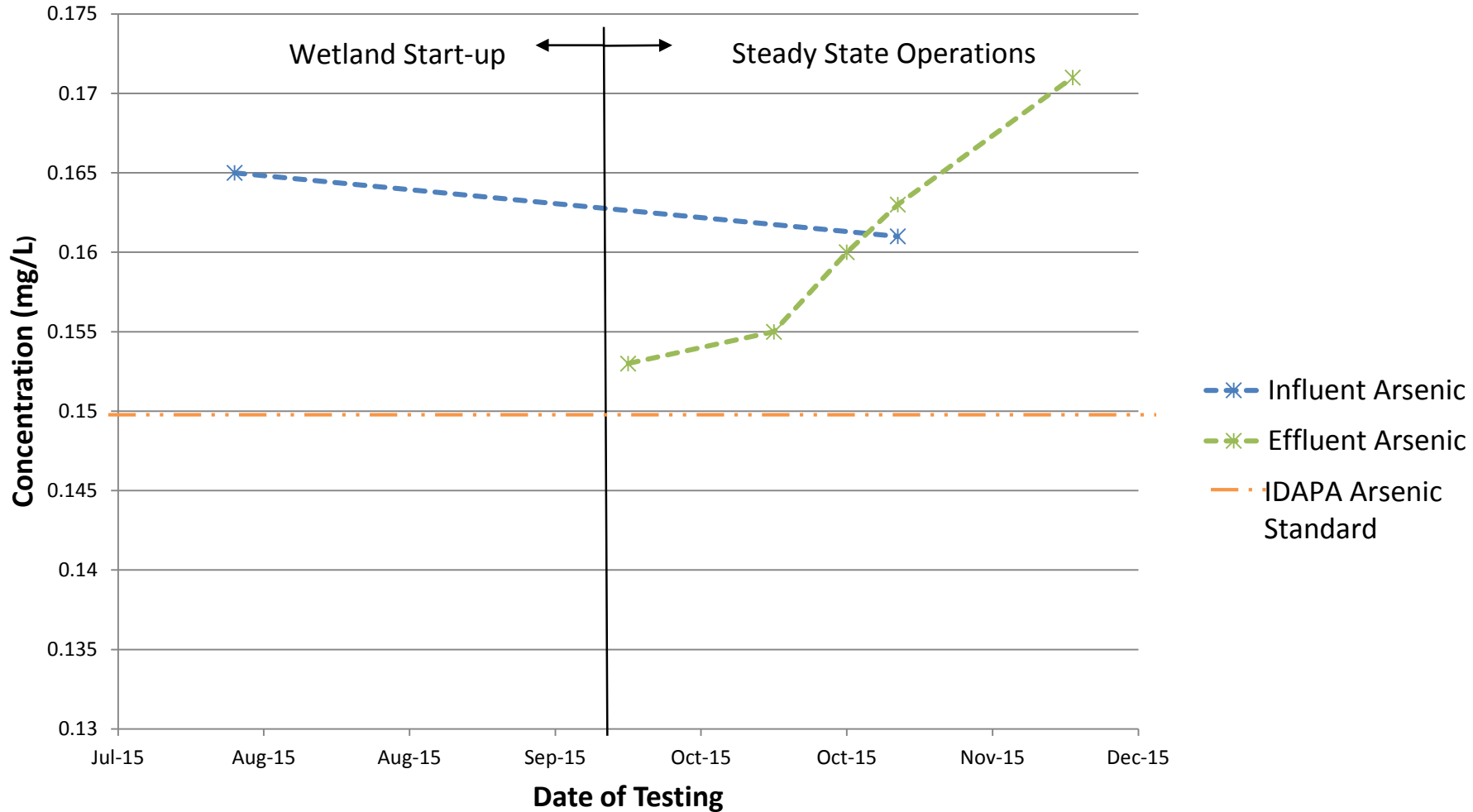


# Bench Testing: Aerobic Wetlands

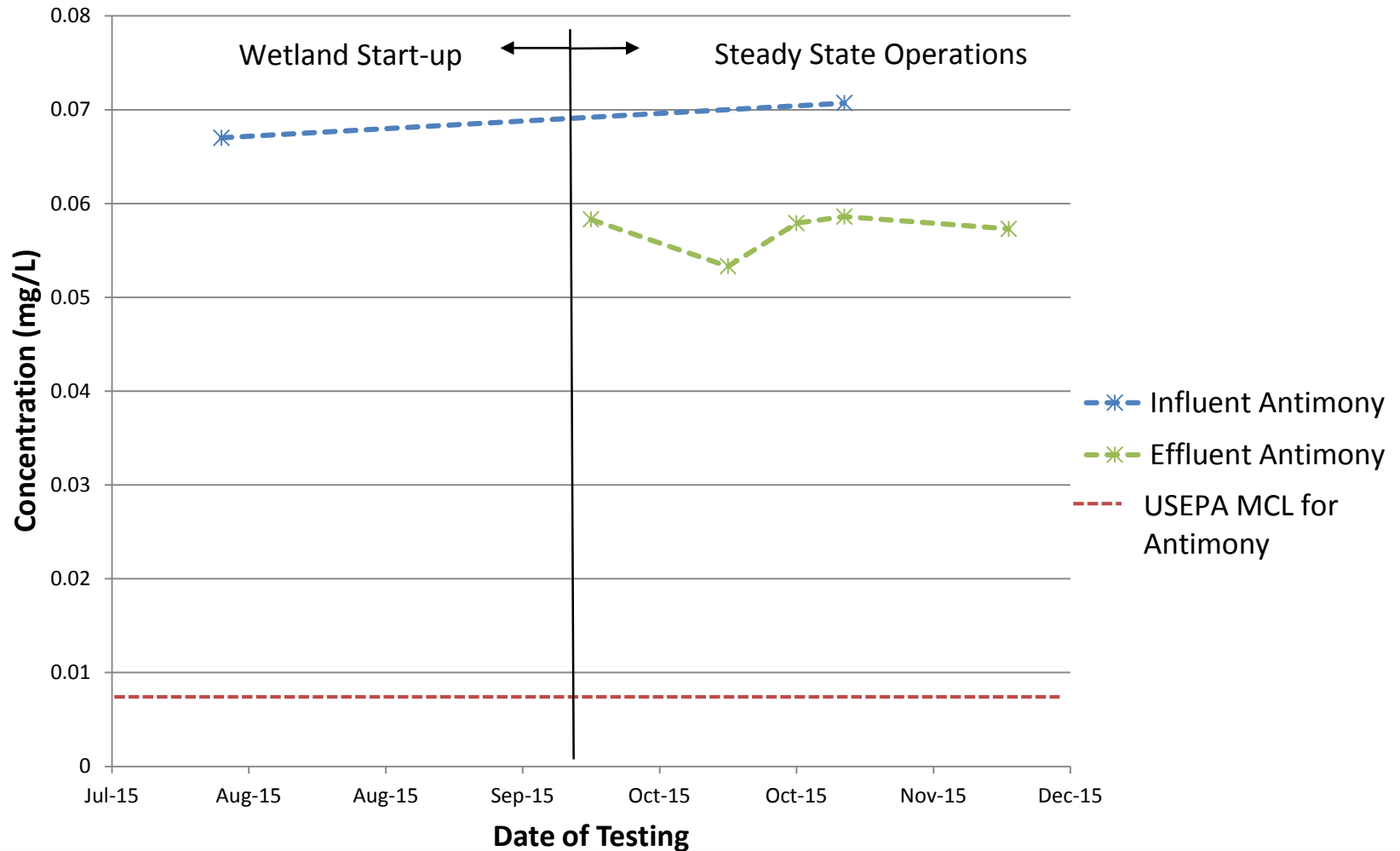
- Two wetlands in series
- 5 day Hydraulic Retention Time (HRT)
- Initial plant selection:
  - Hardstem Bullrush
  - Beaked Sedge
- Final plant selection:
  - Softstem Bullrush
  - Creeping Spikerush
- Top soil mixture for substrate



# Results: Aerobic Wetlands



# Results: Aerobic Wetlands





# Results: Aerobic Wetlands



Wetlands were not effective for removal of Arsenic or Antimony based on water quality:

- Reducing conditions
- Not enough iron present for co-precipitation

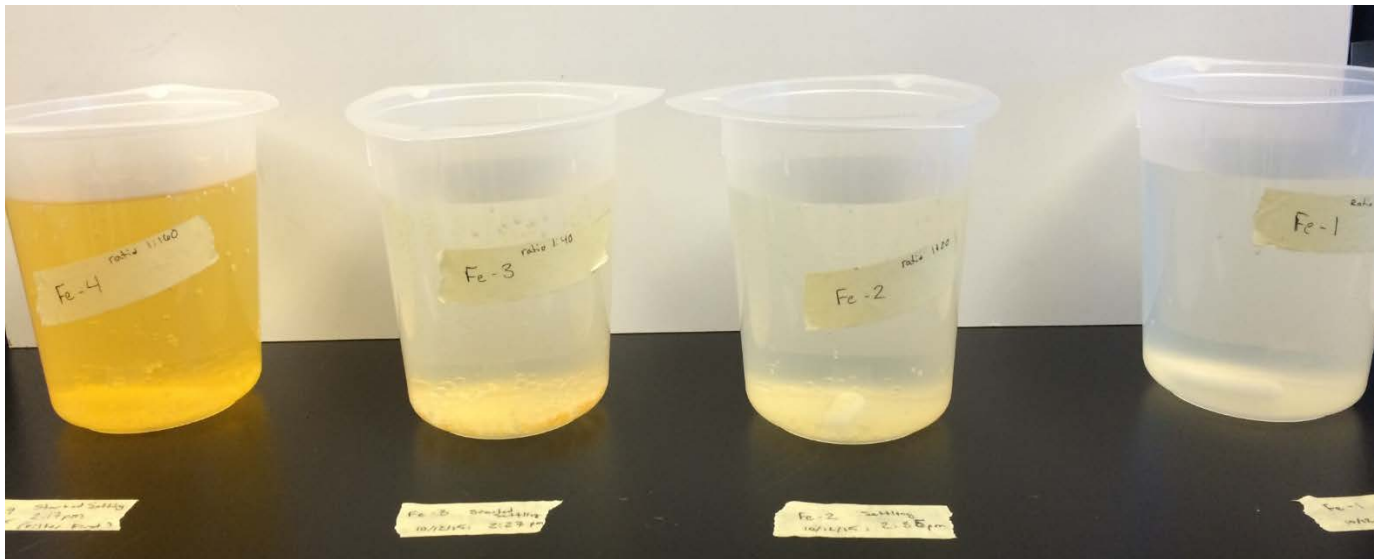
Golder has observed arsenic removal down to 10 ppb in a full scale wetlands with iron present at higher concentrations (California)



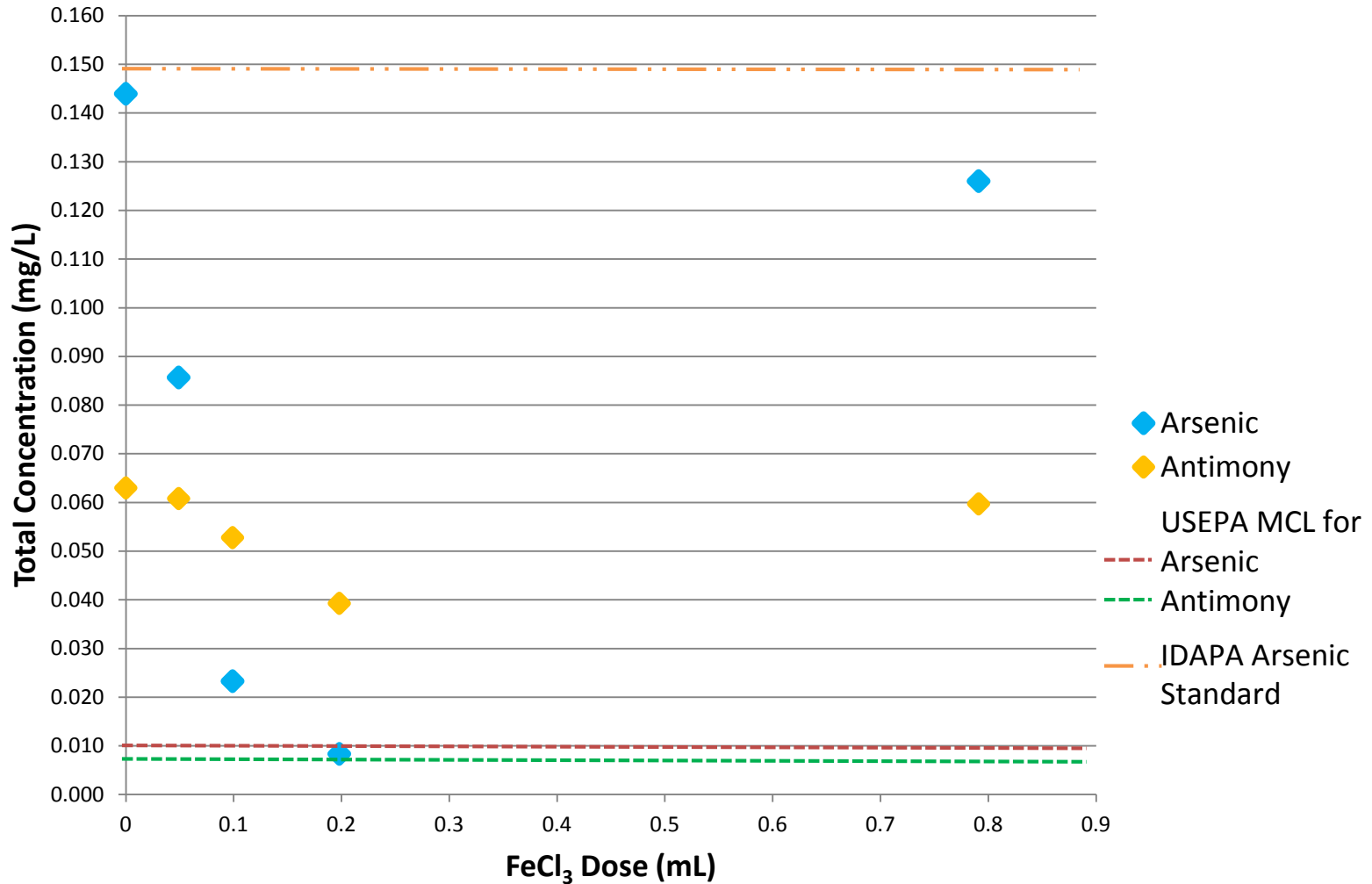
# Bench Testing: Iron Co-precipitation

	FE-1	FE-2	FE-3	FE-4	FE-5
Test	Ratio 1 (10:1)	Ratio 2 (20:1)	Ratio 3 (40:1)	Ratio 4 (160:1)	Control

(moles Iron : moles Arsenic)



# Results: Iron Co-precipitation





# Results: Iron Co-precipitation



Test	FE-1		FE-2		FE-3		FE-4		FE-5
Constituent	Ratio 1 (10:1)	removal	Ratio 2 (20:1)	removal	Ratio 3 (40:1)	removal	Ratio 4 (160:1)	removal	Control
As (Dissolved)	<0.00027	99%	<0.00027	99%	<0.00027	99%	0.00423	78%	0.0188
Sb (Dissolved)	0.0584	11%	0.0493	25%	0.0247	63%	<0.00019	100%	0.0659

pH reduced

## Implementation Requirements

- pH Control
- Chemical Dosing
- Filtration



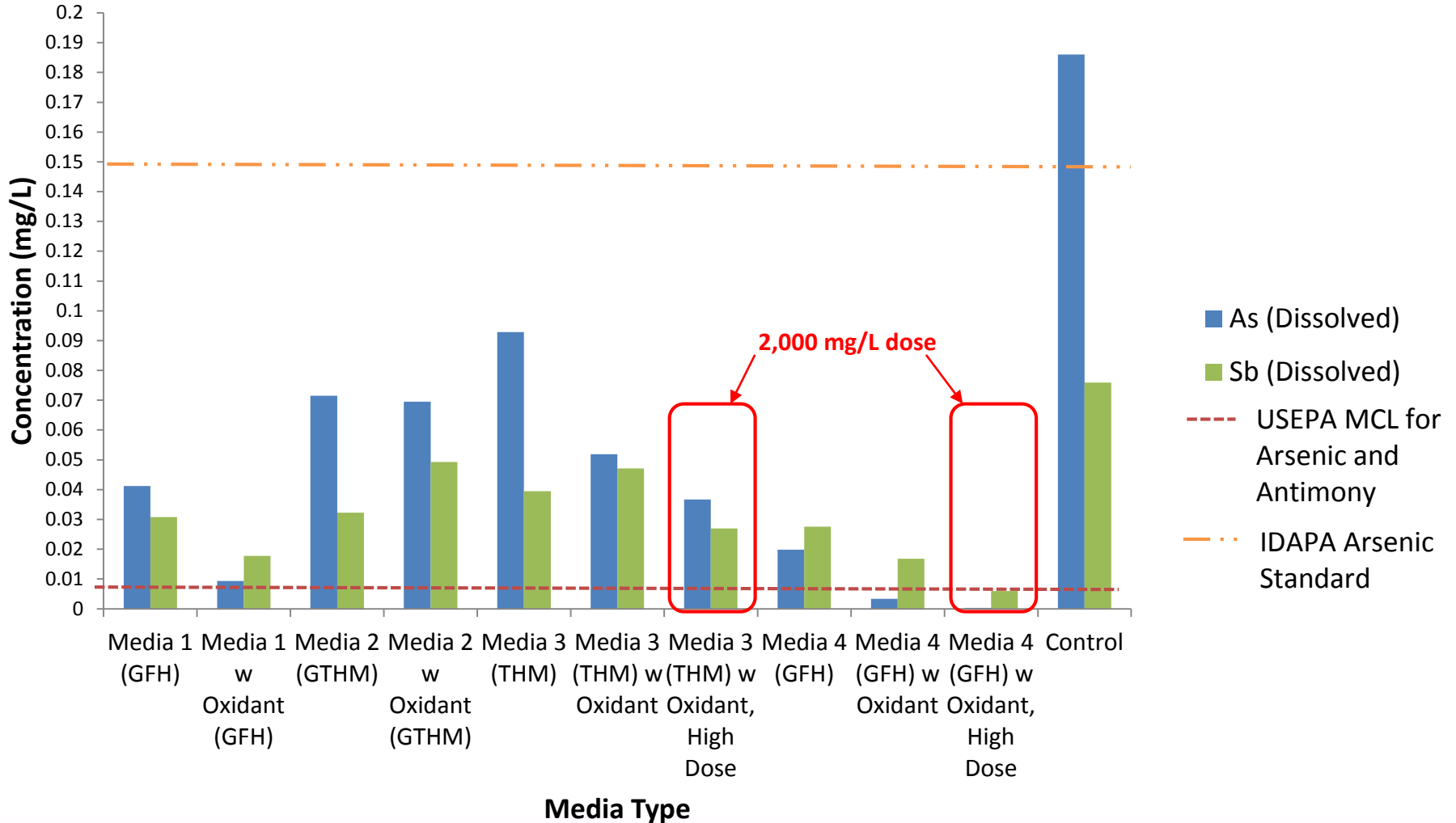
# Bench Testing: Media Absorption



- 2 granular ferric hydroxide media
- 2 titanium based media
- 1 control
- Batch Testing
- Testing with and without Oxidation
- Theoretical dose
- Excess dose



# Results: Media Absorption





# Results: Media Absorption



Test	500mg/L of Media 4				2000mg/L of Media 4	
Constituent	without oxidation	removal	with oxidation	removal	with oxidation	removal
As (Dissolved)	0.0198	89%	0.00333	98%	<0.00027	100%
Sb (Dissolved)	0.0276	64%	0.0168	74%	0.00593	91%

- Pre-oxidation improves media function
- Iron based media has better removal than titanium based media
- When dosed in excess, removal was complete
- Removal is limited by dose/contact time



# Conclusions



## Aerobic Wetlands

- In-effective for treatment of the adit drainage water

## Iron Co-precipitation

- Effective for treatment
- Requires fully active system

## Media Absorption

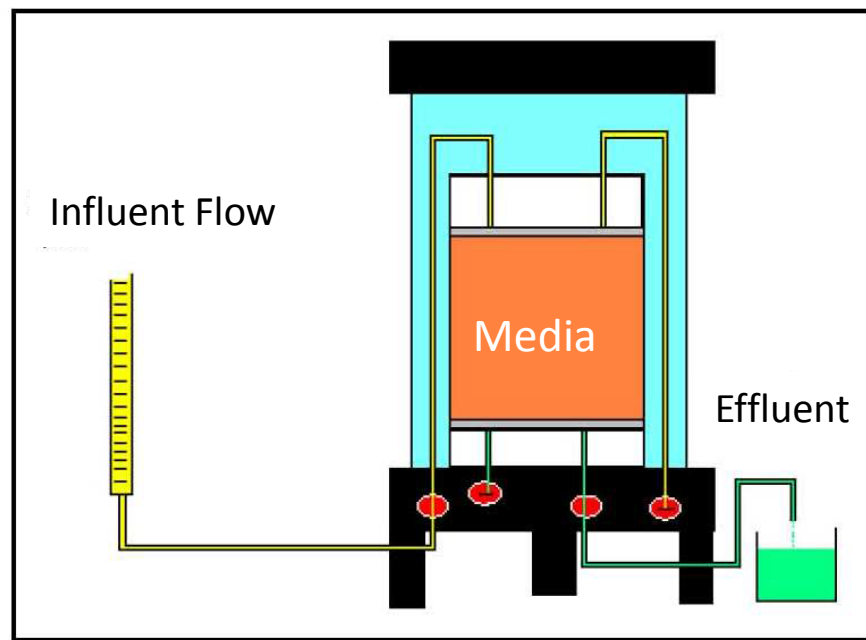
- GFH media effective for treatment
- Able to be implemented in a passive/semi passive configuration
- Further testing required



# Next Steps

## Media Absorption with Oxidation

- Test in a passive configuration
- Establish a required contact time
- Conceptual design



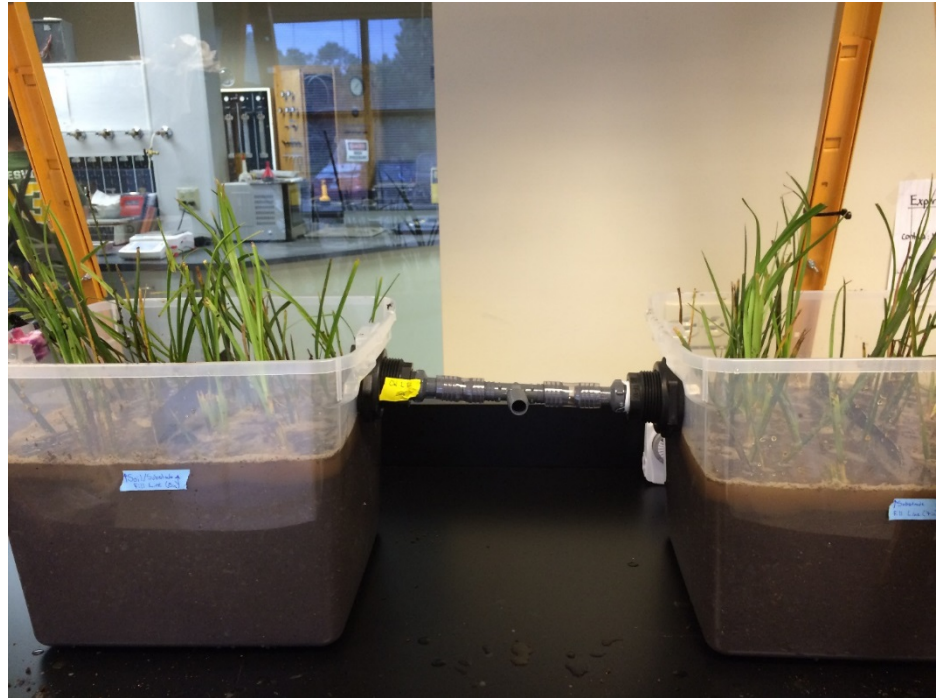


# Thank You!



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# Thank You!

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